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Study in the Variation in the  
Quality of the Steam in the Different  
Stages of the Kerr Turbine

Mechanical Engineering

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STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

BY

JOHN EDWARD EVANS  
AND  
RAFAEL ARCANGEL SOTO

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T H E S I S

FOR THE

DEGREE OF BACHELOR OF SCIENCE

IN

MECHANICAL ENGINEERING

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COLLEGE OF ENGINEERING

UNIVERSITY OF ILLINOIS

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THIS IS TO CERTIFY THAT THE THESIS PREPARED UNDER MY SUPERVISION BY

John Edward Evans and Rafael Arcangel Soto

ENTITLED Study in the Variation in the Quality of the Steam

in the Different Stages of the Kerr Turbine.

IS APPROVED BY ME AS FULFILLING THIS PART OF THE REQUIREMENTS FOR THE

DEGREE OF Bachelor of Science in

Mechanical Engineering.

Instructor in Charge

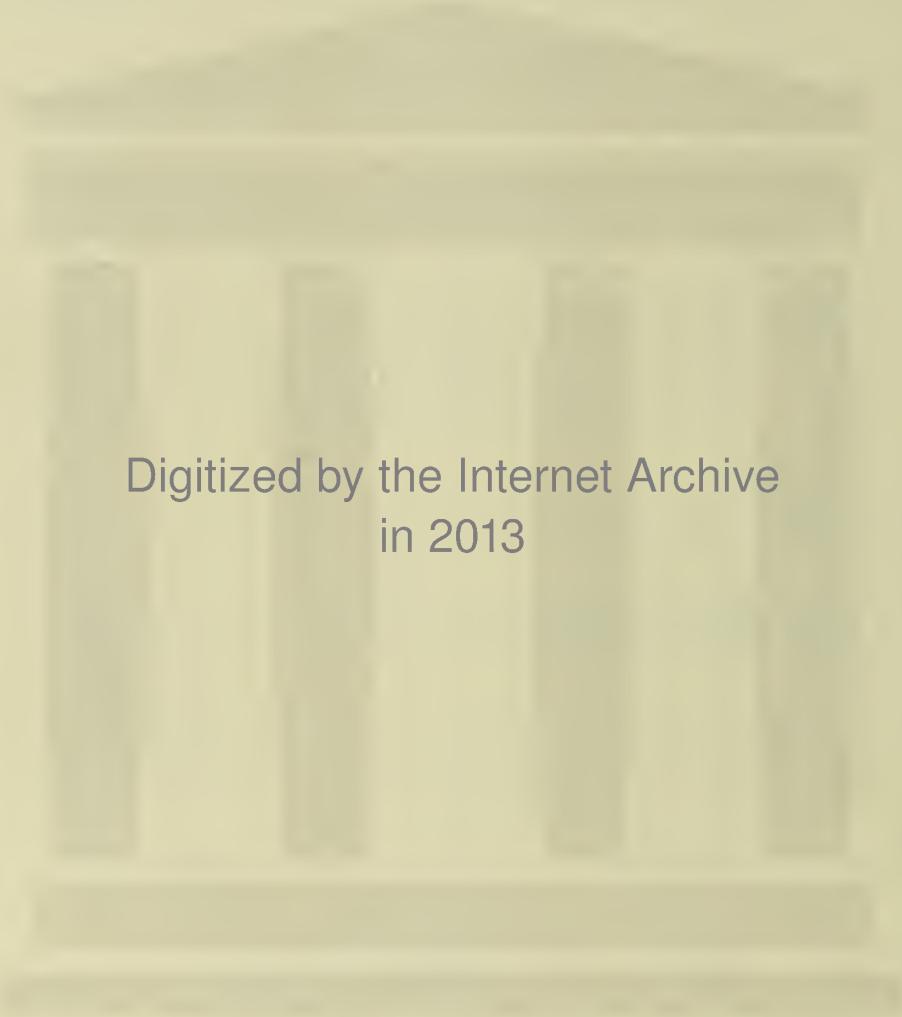
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TABLE OF CONTENTS.

	<u>Page</u>
I. Introduction,.....	2
II. Object of Thesis,.....	2
III. Apparatus,.....	2
IV. Operation of Turbine,.....	4
V. Methods of Conducting the Tests,.....	5
a. Calibration of Gauges,.....	5
b. Preliminary Tests,.....	5
c. Attaching the Calorimeters,.....	5
d. Performance of the Tests,.....	6
VI. Theory,.....	7
VII. Data and Results,.....	
a. Log Sheets,.....	14
b. Result Sheets,.....	29
c. Curve Sheets,.....	31
VIII. Sample Calculations,.....	8
IX. Discussion of Results,.....	9
X. Conclusions,.....	10



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## I. INTRODUCTION.

In the case of the theoretical turbine steam expands adiabatically, i.e., no heat is added or rejected after it once enters the machine. Under these conditions we should have a definite quality at the end of the expansion or even in each stage. In the actual turbine such is not the case. The quality is bound to vary, due to the fact that the amount of heat in the steam is affected by the load applied, and by the friction and windage taking place in the nozzles and in the stages. These tests have been run therefore, to find out experimentally the effect of these factors upon the quality of the steam as it expands through the turbine.

## II. OBJECT OF THESIS.

The object of this thesis is to determine the variation in the quality of the steam in the different stages of a 6-stage, 60 h.p., 18" Kerr turbine, with varying loads.

## III. APPARATUS.

### (a) Apparatus Tested.

The apparatus tested consisted of a 60 h.p. Kerr turbine with the following specifications:

Type of turbine	Multiple stage, velocity.
Maker	Kerr Turbine Co., Wellsville, N.Y.
Shop Number	21
Rated horse power	60
Steam pressure, lb. gage	150
Rev. per min.	3600



Stage number	1	2	3	4	5	6
Absolute pressure, lb. per sq.in.	110.7	74.3	49.8	33.4	22.4	15
Specific volume, cu.ft.	4.002	5.812	8.446	12.27	17.9	26.15
Total nozzle area, sq.in.	0.299	0.435	0.632	0.918	1.338	1.955
Number of nozzles.	6	10	14	20	24	20
Diameter of nozzles, in.	0.252	0.236	0.240	0.242	0.267	0.353
Size of buckets, in.	3/4	3/4	3/4	3/4	3/4	1 1/8
Number of buckets	8 <sup>4</sup>	68				
Diameter of rotors, in.	18					
Diameter of shaft, in.	1 1/2					

(b) Testing Apparatus.

The following is a list of the testing apparatus used in connection with this thesis:

1---Prony brake attached to the turbine.

3---Carpenter's Separating Calorimeters, Serial Nos. 978, 163 and 695.

3---Cans to collect the condensate.

3---Scales to weigh the condensate.

8---Bourdon tube gages.

6 to measure pressure in stages:

	Shop Number	Range
First stage-----	577264	0-100
Second " -----	577265	-30-60
Third " -----	577266	-30-40
Fourth " -----	577267	-30-15
Fifth " -----	577268	-30-10
Sixth " -----	816M218	-30-15



	<u>Shop Number</u>	<u>Range</u>
1 to measure pressure below throttle	577263	0-180
1 to measure pressure in the main	816N206	0-200
1 throttling calorimeter with a 400° F. thermometer to find the quality in the main.		
speedcounter.		

The Prony brake was cooled in the following manner: water entered through a pipe into the inside of the brake pulley. From here it flowed outward, due to centrifugal force, through openings in the rim, passing up through holes into the top block and returning through additional holes. The rubbing surfaces of the blocks were grooved and lubrication was effected by means of soap dissolved in the water.

### III. OPERATION OF THE TURBINE.

Steam enters through the throttle and governor valve under high pressure; then it passes through sets of fixed nozzles, and in so doing its pressure energy is transformed into kinetic energy. The jet from each of the nozzles impinges upon buckets set in the periphery of rotating disks, and these disks, being fast to the turbine shaft, impart their rotation to it. The action at each nozzle is similar to that in a Pelton water wheel.

The scheme of using six stages instead of one has for its purpose the reduction of the peripheral speed. This is accomplished by dividing the total pressure drop between the turbine inlet and the exhaust into six smaller pressure drops which take place in the different stages. The nozzles are so proportioned that the steam velocity is equal at each set of



nozzles. The way the division of the pressure drop is accomplished is as follows:- Steam issuing from the nozzles in the first stage, passes successively through the nozzles in the other stages. The pressure in each stage drops from a high to a lower value just before the jet impinges upon the buckets in the same stage. The drop in pressure causes a corresponding rise in velocity, and this rise of velocity is what produces the impulses upon the buckets of the wheel. This method of compounding is called pressure-compounding, and each drop in pressure constitutes a pressure stage.

#### IV. METHODS OF CONDUCTING THE TESTS.

The following steps were followed in getting the apparatus ready and in running the tests:

##### (a) Calibration of gages.

The Crosby gage tester was used in calibrating the high pressure gages, and the mercury column, with compressed air, in calibrating the low pressure gages. In this respect only the corrected readings are recorded.

##### (b) Preliminary Tests.

The turbine was rated at 60 h.p. for a steam pressure of 150 gage. Since this was not available five preliminary tests were run to find the maximum load that could be carried under existing conditions and also to determine the pressures in the different stages under such conditions.

The different loads were applied by means of the Prony brake mentioned above.

##### (c) Attaching the Calorimeters.

Having decided upon the separating calorimeter as the one



which could be used in all the stages, the housing of the turbine was tapped, calorimeter nipples fitted, and the calorimeters connected. Fig. 1, page 13 shows diagrammatically an end view with the calorimeters attached to the circumference of the housing. In the fifth and sixth stages a trap was used in place of calorimeter 2, due to the fact that water collected at the bottom of the turbine, and this prevented the flow of steam into the calorimeter. The trap was drained by means of a small cock and a rubber tube into a can partially filled with water.

(d) Performance of the Tests.

The sixth stage was the first to be tested, then the fifth, the fourth, and so on. Five tests were run on each stage; for zero load, one-quarter, one-half, three quarter, and full load, as predetermined. Each test lasted thirty minutes, readings being taken every five minutes. Considerable time elapsed between any two tests, thus letting the machine come up to the working condition caused by the new load. In starting a test for any given load in any given stage the first step was to set the brake scales to the required load, and then to apply the brake to the machine until the scale beam was kept in balance. The next step was to bring the pressure in the given stage to what it was in the preliminary test for the same load in the same stage, i.e., to the same pressure which was obtained when the machine was run without any calorimeter attached to it. This second step was accomplished by means of a valve placed between the last stage and the condenser. By adjusting this valve, the pressure in any stage could be increased to any



required value.

## VI. THEORY.

In order to get the quality of the steam existing in each stage of the turbine, three calorimeters were used, as above indicated; one placed near the top, another near the bottom and the third at the side, so arranged that they were approximately  $120^{\circ}$  apart. The quality was determined for each position and the average value taken as the true quality existing in that stage.

Since separating calorimeters were used the quality in each case was determined by means of the formula  $X = \frac{W}{W+S}$ ,

where  $X$  = quality of the steam

$W$  = dry steam passing through the calorimeter and

$S$  = moisture separated in the calorimeter

Let  $X_1$  = quality of the steam in calorimeter 1

$X_2$  = quality of the steam in calorimeter 2 and

$X_3$  = " " " " " " 3

Then  $X = \frac{X_1 + X_2 + X_3}{3}$

The following nomenclature and formulae refer to the tests made upon the lower stages where, on account of moisture a steam trap had to be used.

$W_e$  = pounds of steam collected by condenser.

$W_e \left[ \frac{X_1 + X_2}{2} \right]$  = pounds of dry steam collected by condenser,

where  $w_1 =$  " " " " passing through calorimeter #1, and

$W_3$  = pounds of dry steam passing through calorimeter #3.



$$W = W_e \left[ \frac{X_1 + X_3}{2} \right] + w_1 + w_3$$

$S_e = W_e \left[ 1 - \frac{X_1 + X_3}{2} \right]$  = pounds of moisture entering condenser, where

$S_1$  = pounds of moisture collected in Calorimeter 1.

$S_3$  = " " " " " "

$S_t$  = " " " " " trap.

$$S = S_e + S_1 + S_3 + S_t.$$

$$X = \frac{W}{W+3}$$

#### VII. DATA AND RESULTS.

(a) Log sheets (See pp 14-28)

(b) Result sheets (See pp 29-30)

(c) Curve sheets (See pp 31-33)

#### VIII. SAMPLE CALCULATIONS.

The following calculations are typical of stages 5 and 6, in both of which the trap was used. The data is taken for zero load in the sixth stage.

$$W_e = 377$$

$$w_1 = 2.76 \quad X_1 = \frac{2.76}{2.775} = 0.995$$

$$w_3 = 1.65 \quad X_3 = \frac{1.65}{1.677} = 0.985$$

$$w_t = 0.10$$

$$S_e = 377 \left( 1 - \frac{0.995 + 0.985}{2} \right) = 3.77$$

$$S_1 = 2.76 (1 - 0.995) = 0.014$$

$$S_3 = 1.65 (1 - 0.985) = 0.027$$

$$S_t = M_t = 0.01$$



$$S = 3.911$$

$$\text{quality} = \frac{381.58}{385.421} = 0.99$$

The following calculations are typical of stages 1, 2, 3 and 4, in all of which the three calorimeters were used. The data is taken for the three-quarter load in the second stage.

$$\text{Calorimeter 1 } X_1 = \frac{W_1}{W_1+S_1} = \frac{8.66}{8.66+0.945} = 0.901$$

$$\text{Calorimeter 2 } X_2 = \frac{W_2}{W_2+S_2} = \frac{3.92}{3.92+0.1632} = 0.961$$

$$\text{Calorimeter 3 } X_3 = \frac{W_3}{W_3+S_3} = \frac{6.3}{6.3+0.433} = 0.936$$

$$\text{Average quality} = 0.933$$

#### IX. DISCUSSION OF RESULTS.

The two sets of curves on pages 31 to 32 show in the one case the relation of the quality in the different stages to the initial quality in the main under the various load conditions; and in the second case, they show the variation in the quality from one stage to another. In the sixth stage, the quality varies from 0.99 at zero load to 0.98 at full load, and in the fifth stage, from 0.992 at zero load to 0.989 at full load, thus showing that the quality is practically constant for these two stages, though some irregularity appears in the variation for the intermediate loads. In the fourth and third stages, the quality for the zero and full loads shows a considerable variation, in the fourth stage varying from 0.967 at zero load to 0.926 at full load, and in the third stage from 0.981 at zero load to 0.916 at full load. The quality for the intermediate loads in the third stage varies irregularly. In the



second and first stages, the full load tests were omitted altogether, due to the sticking of the brake on applying the loads. The range of the quality in the second stage was from 0.946 at zero load to 0.933 at three-quarter load, and in the first stage from 0.966 at zero load to 0.979 at three-quarter load.

In running the tests in stages 5 and 6 the quality of steam entering the condenser was taken as the average of that determined by calorimeters #1 and #3. It might be well here to note that this is only approximately correct for it was found out later that the quality varied in each stage, being higher at the top and lower at the bottom of the stage. The two calorimeters used were connected at the middle and top of the stage so this quality assumed is somewhat higher than it should be.

#### X. CONCLUSIONS.

(a) In any stage, as the load increases, the quality decreases, and vice - versa; i.e., the quality of the steam varies inversely as the load applied. This conclusion would naturally be expected, considering the fact that the greater the load the more work the turbine would have to do; and this work could only come from the heat in the steam, according to the transformation law of energy.

(b) The quality decreases as we go from the top to the bottom of the turbine. This is due to the fact that in running the turbine a considerable amount of water is separated from the steam through the churning action in the stages, and as this



drips down over the walls the steam in the lower parts becomes denser and denser, until at the bottom there is nothing but a mixture of water and steam.

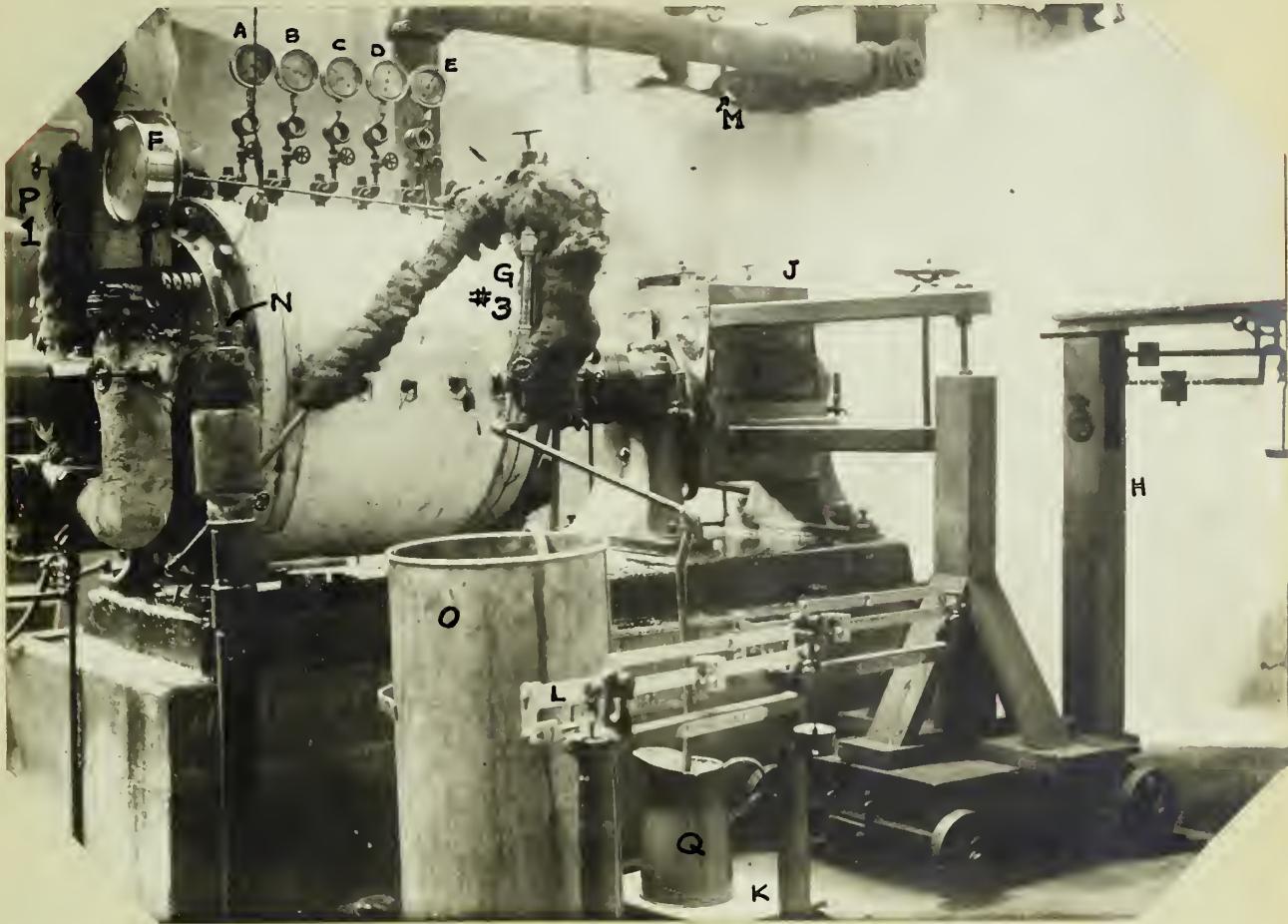
(c) As the steam flows from stage 1 to stage 6, the quality increases due to friction in the nozzles and blades and windage in the stages.



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

PLATE #1.

VIEW SHOWING THE TURBINE WITH CALORIMETER #3  
ATTACHED TO THE FIRST STAGE AND THE OTHER INSTRUMENTS  
IN THEIR RESPECTIVE POSITIONS.



A—STEAM GAGE FOR DETERMINING PRESSURE IN STAGE #1

B—	"	"	"	"	"	"	"	2
C—	"	"	"	"	"	"	"	3
D—	"	"	"	"	"	"	"	4
E—	"	"	"	"	"	"	"	5
F—	"	"	"	"	"	"	"	MAIN

G—SEPARATING CALORIMETER #3

H—PRONY BRAKE SCALE

J—PRONY BRAKE

K—SCALE FOR WEIGHING WATER SEPARATED FROM STEAM IN CAL.#3

L—" " " EXHAUST STEAM FROM CALORIMETER #3

M—VALVE IN EXHAUST FOR PRODUCING DESIRED BACK PRESSURE

N—THERMOMETER CUP IN THROTTLING CALORIMETER IN MAIN LINE

O—CONDENSATE CAN FOR CAL.#3

P—CALORIMETER #1

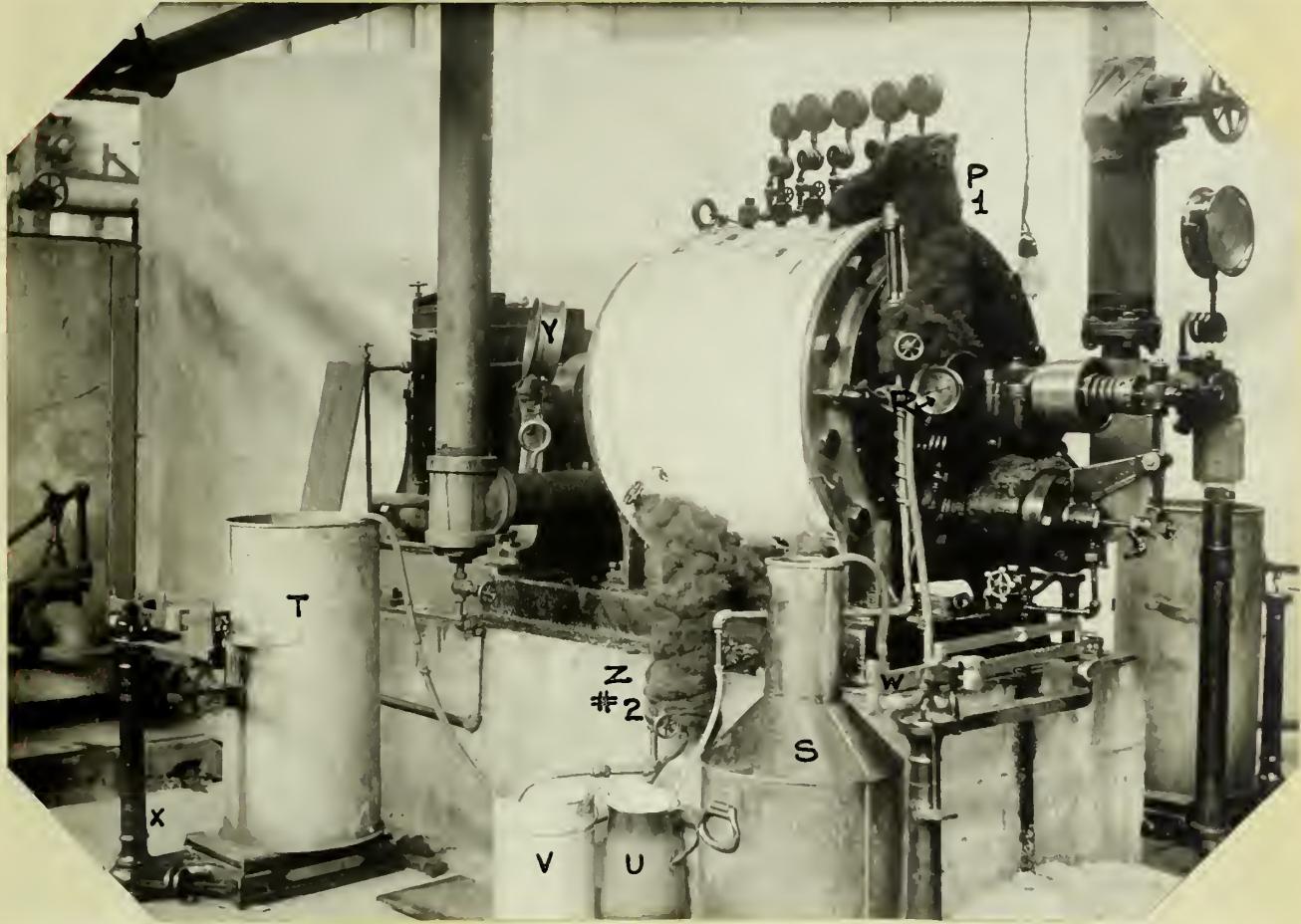
Q—SEPARATED WATER CAN FOR CAL.#3



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

PLATE #2

VIEW SHOWING THE TURBINE FROM THE OPPOSITE SIDE TO THAT SHOWN IN PLATE #1 AND SHOWING CALORIMETERS #1 AND #3 ATTACHED TO STAGE #1 AND THE OTHER INSTRUMENTS IN THEIR RESPECTIVE POSITIONS.



P—CALORIMETER #1

R—GAGE BELOW THROTTLE

S—EXHAUST STEAM CAN FOR CAL. #1

T— " " " " " " 2

U—SEPARATED WATER " " " 1

V— " " " " " " 2

W—SCALE FOR EXHAUST STEAM FROM CAL #1

X— " " " " " " " 2

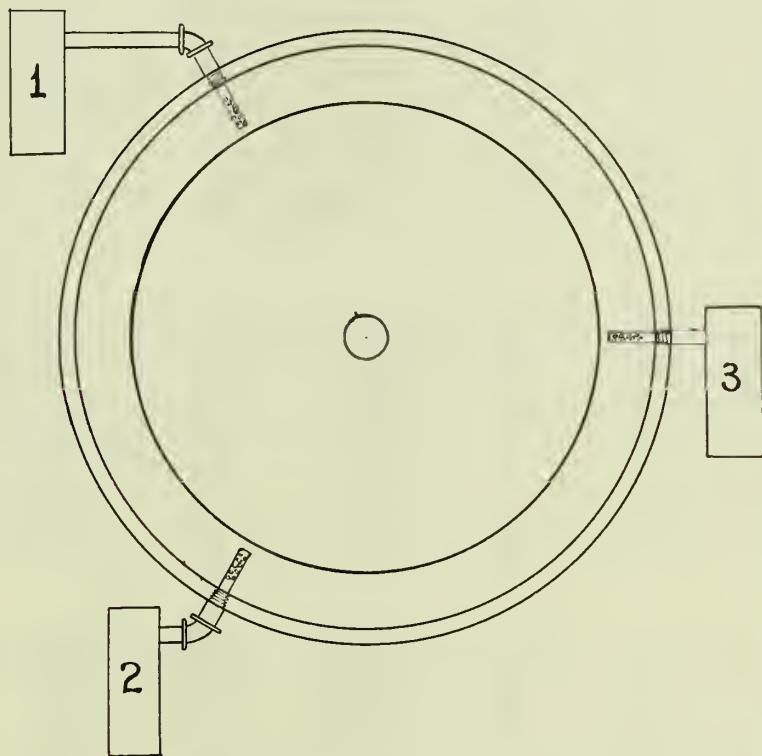
Y—GAGE IN SIXTH STAGE

Z—CALORIMETER #2



## PLATE # 3

SKETCH SHOWING SECTION OF TURBINE AND  
LOCATION OF THE CALORIMETERS WITH RESPECT TO  
THE HOUSING, AND THE NUMBER ASSIGNED TO EACH  
CALORIMETER.





(14)

STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE.

PRELIMINARY TESTS FOR DETERMINING, WITHOUT CALORIMETERS  
INSERTED, THE PRESSURES IN THE DIFFERENT STAGES—

LOAD	R.P.M	PRESSURES.						
		BELOW THROTTLE	IN STAGES					
			1	2	3	4	5	6
0	3600	30	16.6	10	6.0	3.7	2.8	2.0
"	"	31	16.7	10	6.1	3.8	2.85	2.0
"	"	31	16.6	10	6.2	3.8	2.9	2.0
"	"	31	16.7	10	6.1	3.8	2.9	2.0
"	"	31	16.8	10	6.2	3.9	2.9	2.1
"	"	31	16.7	10	6.2	3.9	2.9	2.1
"	"	31	16.7	10	6.2	3.9	3.0	2.1
$\frac{1}{4}$	3600	50	26	16.7	10.1	5.9	3.3	2.0
"	"	52	27.1	17.1	10.5	6.1	3.8	2.0
"	"	53	28.	18.2	11.0	6.2	3.8	2.0
"	"	53	27.5	18.0	10.8	6.1	3.7	2.0
"	"	52	27.	17.5	10.8	6.1	3.7	2.0
"	"	53	27.5	18.0	10.8	6.1	3.7	2.0
"	"	53	27.5	18.0	10.9	6.1	3.8	2.0
$\frac{1}{2}$	3600	70	41.	27	16	8.9	4.7	2.0
"	"	70	41	26.8	16	8.9	4.7	2.0
"	"	70	40.5	26.5	16	8.9	4.7	2.1
"	"	70	41	27.0	16	9.0	4.8	2.0
"	"	70	41	26.9	16	8.9	4.7	2.0
"	"	70	41	27.	16	8.9	4.7	2.0
"	"	70	41	27.	16	9.0	4.8	2.0
$\frac{3}{4}$	3600	95	54.5	35.5	22.	11.9	6	1.9
"	"	93	54.	35.4	21.9	11.8	6	1.9
"	"	93	54.	35.2	22	11.8	6	1.9
"	"	93	54.	35.4	22	11.8	6	1.9
"	"	93	54.	35.3	22	11.8	6	1.9
"	"	94	54.	35.4	22	11.8	6	1.9
"	"	93	54.	35.4	22	11.8	6	1.9
FULL	3600	112	66	45.	27	15	8.2	2
"	"	115	67	45.2	28	15	8	2
"	"	114	67	45.2	28	15	8	2
"	"	115	67	45.2	28	15	8	2
"	"	115	67	45.2	28	15	8	2
"	"	114	67	45.2	28	15	8	2
"	"	115	67	45.2	28	15	8	2



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE I  
LOAD O  
BAROMETER 29.791 " Hg.

STAGE	LOAD	BAROMETER	CALORIMETER #1	CALORIMETER #2				TEMP. IN MAIN CAL. OF	PRESSURES # GAUGE	STAGE	
				STEAM CONDENSED READING LB	WATER CONDENSED READING LB	STEAM GAUGE WATER CONDENSED READING LB	STEAM GAUGE WATER CONDENSED READING LB				
513.20	.000	—	123.55	.000	—	118.29	.000	3600	284	134	34
513.74	.006	—	124.00	.003	—	118.92	.001	"	284	134	34
514.56	.013	—	124.26	.004	—	119.51	.002	"	280	134	34
515.48	.015	—	124.68	.007	—	120.14	.004	"	278	133	36
516.24	.023	—	125.05	.012	—	120.83	.005	"	278	134	35
517.14	.025	—	125.50	.014	—	121.46	.011	"	279	137	36
518.51	.028	—	125.93	.016	—	122.10	.016	"	278	136	35

STAGE I  
LOAD  $\frac{1}{4}$   
BAROMETER 29.469 " Hg.

511.06	.000	—	119.98	.002	—	116.85	.010	—	3540	271	113	54	27.3	18.2	10.5	5.6	3.4	1.4
512.16	.027	—	120.56	.005	—	117.76	.015	—	3600	270	117	"	"	18.1	"	5.6	3.4	1.5
513.56	.049	—	121.09	.013	—	118.68	.030	—	3600	269	123	"	"	18.1	"	5.7	3.4	1.5
514.44	.079	—	121.71	.029	—	119.60	.052	—	3600	270	130	"	"	18.0	"	5.7	3.5	1.6
516.08	.096	—	122.30	.037	—	120.48	.075	—	3600	272	128	"	"	18.0	"	5.7	3.5	1.6
517.16	.109	—	122.82	.056	—	121.42	.090	—	3600	275	119	"	"	18.0	"	5.6	3.4	1.4
518.36	.123	—	123.42	.064	—	122.40	.106	—	3600	274	120	"	"	18.0	"	5.6	3.5	1.5



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE I  
LOAD  $\frac{1}{2}$   
BAROMETER 29.471 " Hg.

STAGE	LOAD	BAROMETER	CALORIMETER #1												CALORIMETER #2												CALORIMETER #3												PRESSURES IN STAGES																																																																																													
			STEAM GAUGE			WATER CONDENSED			WATER GAUGE			CONDENSED			WATER DRAINED			STEAM GAUGE			CONDENSED			WATER DRAINED			MAIN CAL. OF			R.P.M.			TEMP. IN BFLOW			IN MAIN THROTTLE			IN CAL.			TEMP. IN MAIN			IN MAIN THROTTLE			# GAUGE																																																																																				
LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB																																																																																						
120.12	.000	—	534.74	.014	—	119.48	.025	—	3600	278	130	83	44.0	30.0	17.6	9.6	5.3	2.1	120.77	.011	—	535.64	.040	—	120.61	.054	—	"	278	126	78	41.0	27.6	16.0	8.8	4.7	1.9	121.54	.022	—	536.98	.068	—	121.86	.088	—	"	277	122	76	41.0	27.5	16.0	8.8	4.7	1.8	122.26	.048	—	538.98	.104	—	123.00	.129	—	"	271	127	77	41.0	27.6	16.0	8.8	4.7	1.9	122.96	.064	—	539.95	.142	—	124.26	.166	—	"	270	131	75	41.0	27.3	15.8	8.5	4.5	1.8	123.71	.083	—	541.64	.174	—	125.39	.200	—	"	272	131	75	41.0	27.0	15.5	8.4	4.5	1.9	124.40	.101	—	543.35	.205	—	126.59	.236	—	"	273	132	75	41.0	27.0	15.5	8.4	4.5	1.9

STAGE I  
LOAD  $\frac{3}{4}$   
BAROMETER 29.790 " Hg.

525.98	.022	—	119.81	.026	—	120.26	.020	—	3600	284	125	97	54.0	36.4	22.0	11.8	6.4	2.1
527.82	.057	—	120.89	.050	—	121.74	.060	—	"	278	127	97	"	36.5	22.0	11.8	6.4	2.4
529.90	.090	—	121.82	.072	—	123.23	.108	—	"	278	126	97	"	36.3	22.0	11.8	6.4	2.1
531.90	.125	—	122.66	.085	—	124.62	.158	—	"	278	130	97	"	36.0	22.0	12.0	6.8	2.1
533.82	.161	—	123.62	.100	—	126.08	.207	—	"	278	127	96	"	36.0	22.0	12.0	6.8	2.8
535.72	.190	—	124.52	.121	—	127.50	.238	—	"	283	123	96	"	36.0	22.1	12.1	6.8	2.7
537.80	.218	—	125.44	.140	—	128.93	.269	—	"	280	126	97	"	36.1	22.1	12.0	6.8	2.7



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE.

STAGE 2.  
LOAD  
BAROMETER 28.873 " Hg

CALORIMETER #1	CALORIMETER #2			CALORIMETER #3			TEMP. IN MAIN CAL. OF	PRESSURE IN MAIN THROTTLE	PRESSURE S.			# GAUGE.					
	STEAM CONDENSED READING LB.	GAUGE WATER DRAINED CONDENSED READING LB.	STEAM GAUGE WATER DRAINED CONDENSED READING LB.	STEAM GAUGE WATER DRAINED CONDENSED READING LB.	WATER DRAINED CONDENSED READING LB.	R.P.M.			IN MAIN CAL. OF	IN MAIN CAL. OF	IN MAIN CAL. OF						
508.53 .026	7.34	114.51	.070	4.02	115.22	.014	412	3600	277	134	35	17.0	10.0	5.1	3.0	1.0	0
509.04 .045	"	114.87	.118	"	115.80	.038	"	"	277	137	35	17.0	10.0	5.1	3.0	1.0	0
509.70 .059	"	115.16	.163	"	116.27	.059	"	"	280	134	35	17.0	10.0	5.1	3.0	1.2	0
510.49 .085	"	115.43	.200	"	116.82	.081	"	"	279	139	36	17.0	10.0	5.1	3.0	1.2	0
511.22 .093	"	115.76	23. <sup>ET</sup> <sub>.004</sub>	"	117.35	.098	"	"	279	132	36	17.0	10.0	5.1	2.9	1.2	0
512.00 .099	"	116.09	.020	"	117.85	.109	"	"	278	128	35	17.0	10.0	5.1	2.9	1.2	0
512.75 .110	7.34	116.37	.065	4.25	118.37	.125	412	"	276	130	36	17.0	10.0	5.1	2.9	1.1	0

<sup>ET</sup> = EMPTIED TO.

STAGE 2.  
LOAD  
BAROMETER 28.864 " Hg

501.56 .015	7.71	117.94	.032	4.76	114.62	.029	478	3600	273	124	52	27.0	17.5	10.4	6.0	3.7	1.9
502.18 .070	"	118.31	.130	"	115.26	.078	"	"	274	125	52	27.0	17.5	10.4	6.0	3.7	1.9
503.89 .120	"	118.76	.220	"	115.95	.112	"	"	275	122	52	26.8	17.5	10.3	6.0	3.5	1.9
504.50 .178	"	119.14	27. <sup>ET</sup> <sub>.046</sub>	"	116.68	.150	"	"	274	122	52	27.0	17.5	10.3	6.0	3.5	1.9
505.10 273. <sup>ET</sup> <sub>.048</sub>	"	119.64	.15	"	117.31	.193	"	"	273	127	52	27.0	17.5	10.3	6.0	3.6	1.9
505.72 .084	"	120.00	23. <sup>ET</sup> <sub>.048</sub>	"	117.97	.241. <sup>ET</sup> <sub>.05</sub>	"	"	273	132	52	27.0	17.5	10.3	6.0	3.6	1.9
506.94 .142	7.92	120.36	.121	5.19	118.72	.079	496	"	272	135	52	27.0	17.5	10.3	6.0	3.6	2.0



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE 2  
LOAD  $\frac{1}{2}$   
BAROMETER 28.864" Hg.

CALORIMETER #1				CALORIMETER #2				CALORIMETER #3				PRESSURES					
STEAM GAUGE CONDENSED READING LB	WATER CONDENSED READING LB	R.P.M.	IN MAIN CAL. OF	TEMP. IN MAIN THROTTLE	IN MAIN THROTTLE	IN MAIN THROTTLE	IN MAIN THROTTLE	IN MAIN THROTTLE	IN MAIN THROTTLE	# GAUGES							
516.27 .048	8.31	124.41	.078	5.70	119.04	.020	5.46	3600	278	123	73	27.0	17.5	10.4	6.0	3.7	2.0
517.12 .—	" 126.00	—	" 119.84	—	" 120.73	—	" 121.66	—	275	125	72	27.0	"	10.4	6.0	3.7	1.9
518.42 .—	" 126.55	—	" 121.66	—	" 121.66	—	" 122.56	—	273	129	73	26.8	"	10.3	6.0	3.5	2.0
519.58 .—	" 127.05	—	" 123.49	—	" 123.49	—	" 124.46	.180	274	133	73	27.0	"	10.3	6.0	3.5	2.0
521.10 .—	" 127.63	—	" 125.12	—	" 125.12	—	" 126.21	.138	273	138	74	27.0	"	10.3	6.0	3.6	2.0
521.99 .—	" 128.06	—	" 126.66	—	" 126.66	—	" 127.21	.140	275	138	73	27.0	"	10.3	6.0	3.6	2.0
523.61 .096	8.84	128.61	.165	6.71	124.46	.180	5.61	"	274	133	73	27.0	"	10.3	6.0	3.6	2.0

STAGE 2  
LOAD  $\frac{3}{4}$   
BAROMETER 28.860" Hg.

508.00 .045	9.38	124.30	.068	7.49	119.91	.035	6.06	3600	279	126	95	54.5	35.4	21.5	11.8	6.0	2.1
509.32 .—	" 125.03	—	" 121.12	—	" 122.11	—	" 123.19	—	279	127	97	54.5	"	21.5	11.8	6.0	2.1
510.63 .—	" 125.64	—	" 123.19	—	" 124.13	—	" 125.17	—	280	122	96	54.0	"	21.0	11.7	6.0	1.9
512.38 .—	" 126.31	—	" 124.13	—	" 125.17	—	" 126.21	.138	279	124	94	54.3	"	21.2	11.7	6.0	1.9
513.64 .—	" 126.93	—	" 125.17	—	" 126.21	.139	" 127.22	.141	280	122	95	54.0	"	21.0	11.7	6.0	1.9
515.00 .—	" 127.59	—	" 126.21	.138	" 127.22	.141	" 128.22	.270	277	121	97	54.5	"	21.2	11.8	6.0	1.9
516.66 .160	10.21	128.22	.270	8.92	126.21	.138	6.39	"	277	121	97	54.5	"	21.3	11.8	6.0	1.9



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE 3  
LOAD O  
BAROMETER 29.196 " Hg.

CALORIMETER #1	CALORIMETER #2	CALORIMETER #3	TEMP. R.P.M.	IN MAIN CAL. °F	IN MAIN THROTTLE	PRESSURES									
						STEAM CONDENSED READING LB	WATER CONDENSED READING LB	STEAM GAUGE DRAINED LB	WATER CONDENSED READING LB	WATER DRAINED LB	IN MAIN STAGES	IN MAIN STAGES			
103.19 .000	—	68.75 .003	—	68.62 .000	—	3600	270	129	36	18.0	12.0	6.2	3.5	2.1	.8
103.84 .002	—	69.00 .010	—	69.15 .001	—	"	270	128	36	18.0	11.6	"	"	2.1	.8
104.73 .003	—	69.26 .016	—	69.70 .002	—	"	270	128	37	18.0	11.0	"	"	2.1	.8
105.11 .004	—	69.48 .022	—	70.01 .009	—	"	269	131	37	18.5	11.9	"	"	2.1	.7
105.66 .005	—	69.68 .029	—	70.55 .100	—	"	270	134	38	18.5	12.0	"	"	2.1	.7
106.33 .006	—	69.93 .041	—	70.95 .140	—	"	272	135	37	18.5	12.0	"	"	2.2	.7
107.23 .009	—	70.17 .050	—	71.41 .150	—	"	270	133	38	18.5	12.0	"	"	2.2	.6

STAGE 3  
LOAD  $\frac{1}{4}$   
BAROMETER 29.310" Hg.

118.28 .010	—	73.24 .003	—	74.00 .017	—	3600	272	122	59	35.2	24.8	16.0	11.0	8.3	0.0
119.24 .059	—	73.62 .058	—	74.65 .045	—	"	273	124	62	35.2	24.3	16.0	11.0	8.3	"
120.12 .093	—	74.00 .087	—	75.30 .077	—	"	274	123	61	35.0	24.0	16.0	11.0	8.2	"
121.01 .123	—	74.40 .124	—	76.06 .102	—	"	276	120	58	35.1	24.3	16.0	11.0	8.2	"
121.86 .169	—	74.80 .158	—	76.70 .136	—	"	274	120	63	34.9	24.1	15.9	11.1	8.8	"
122.90 .211	—	75.24 .198	—	77.44 .174	—	"	271	125	62	35.0	24.3	16.0	11.7	9.0	"
123.71 .260	—	75.67 .228	—	78.09 .210	—	"	274	129	62	35.0	24.5	16.0	11.8	9.0	"



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE      3  
LOAD       $\frac{1}{2}$   
BAROMETER 29.207 " Hg.

CALORIMETER #1	CALORIMETER #2				CALORIMETER #2				TEMP				PRESSURE S				
	STEAM GAUGE CONDENSED READING	WATER CONDENSED READING	STEAM CONDENSED READING	WATER CONDENSED READING	STEAM GAUGE CONDENSED READING	WATER CONDENSED READING	WATER GAUGE CONDENSED READING	WATER CONDENSED READING	R.P.M.	IN MAIN CAL. OF	IN MAIN	IN MAIN THROTTLE	IN MAIN	IN MAIN	IN MAIN	IN MAIN	# GAUGE
112.85 .003	—	71.16	.098	5.48	68.47	.020	—	3600	272	132	73	41.5	28.0	16.0	8.9	4.8	2.0
113.73 .010	—	71.53	—	"	69.12	.025	—	"	272	136	76	41.5	28.0	"	9.0	4.8	2.1
114.73 .019	—	72.00	—	"	69.80	.030	—	"	274	134	74	41.4	28.0	"	9.0	4.8	1.9
115.80 .029	—	72.42	—	"	70.52	.041	—	"	275	133	74	41.2	27.9	"	9.0	4.8	1.9
116.65 .035	—	72.82	—	"	71.27	.065	—	"	271	132	75	41.4	27.6	"	9.0	5.0	2.1
117.59 .045	—	73.22	—	"	71.84	.084	—	"	271	134	74	41.3	27.6	"	9.0	5.0	2.1
118.49 .055	—	73.62	.270	6.14	72.44	.093	—	"	271	133	75	41.3	27.6	"	9.0	5.0	2.0

STAGE      3  
LOAD       $\frac{3}{4}$   
BAROMETER 29.218 " Hg.

110.05 .000	—	70.47	.070	4.820	75.08	.005	—	3600	279	119	95	54.5	37.4	22.0	12.0	6.6	2.3
111.07 .015	—	70.89	—	"	75.91	.015	—	"	276	124	96	54.0	37.0	"	"	6.5	2.3
112.24 .025	—	71.36	—	"	76.73	.039	—	"	275	131	96	54.0	37.0	"	"	6.5	2.3
113.39 .033	—	71.89	—	"	77.63	.059	—	"	277	133	97	54.3	37.0	"	"	6.5	2.2
114.50 .041	—	72.39	—	"	78.42	.083	—	"	279	130	96	54.0	37.0	"	"	6.5	2.3
115.59 .050	—	72.84	—	"	79.19	.106	—	"	280	126	96	54.0	37.0	"	"	6.5	2.3
116.71 .058	—	73.34	.250	5.276	79.97	.130	—	"	280	128	96	54.0	37.0	"	"	6.5	2.3



## STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE 3  
LOAD FULL  
BAROMETER 29.144 " Hg

PRESSURES										# GAUGE								
CALORIMETER #1					CALORIMETER #2					CALORIMETER #3					IN STAGES			
STEAM CONDENSED READING LB	WATER CONDENSED READING LB	STEAM CONDENSED READING LB	WATER CONDENSED READING LB	STEAM CONDENSED READING LB	WATER CONDENSED READING LB	STEAM CONDENSED READING LB	WATER CONDENSED READING LB	R.P.M.	TEMP IN MAIN CAL. OF	IN MAIN THROTTLE								
102.26	.014	—	61.93	.097	4.93	73.32	.009	—	3600	281	130	118	67.0	46.0	28.0	15.5	8.8	3.6
103.54	.032	—	62.49	—	"	74.28	.035	—	"	279	132	118	67.0	46.0	28.0	15.5	8.8	3.4
104.73	.048	—	63.02	—	"	75.17	.067	—	"	282	127	117	67.0	45.5	"	15.3	8.5	3.5
105.16	.068	—	63.66	—	"	76.13	.090	—	"	280	133	121	66.8	46.0	"	15.4	8.5	3.4
106.47	.081	—	64.17	—	"	77.10	.123	—	"	281	133	120	67.0	46.0	"	15.5	8.7	3.5
107.67	.097	—	64.71	—	"	78.00	.142	—	"	283	127	116	67.0	46.0	"	15.5	8.8	3.3
109.85	.120	—	65.24	.158	5.76	79.00	.166	—	"	283	122	117	67.0	46.0	"	15.5	8.5	3.2

STAGE 4  
LOAD 0  
BAROMETER 29.154 " Hg.

112.86	.000	—	68.55	.033	—	72.43	.017	—	3600	279	135	37	19.5	12.0	6.7	3.8	2.4	.9
113.41	.002	—	68.63	.038	—	72.81	.012	—	..	276	138	37	19.0	12.3	7.0	3.8	2.5	..
114.00	.003	—	68.75	.048	—	73.18	.018	—	..	278	139	37	19.0	12.4	6.9	3.8	2.5	..
114.48	.005	—	68.86	.058	—	73.58	.026	—	..	279	140	37	19.0	12.3	6.9	3.8	2.4	..
115.00	.009	—	68.97	.065	—	73.95	.035	—	..	278	140	36	19.5	12.0	6.9	3.8	2.5	..
115.51	.014	—	69.10	.072	—	74.32	.051	—	..	280	135	36	19.5	12.0	6.8	3.7	2.4	..
116.16	.022	—	69.16	.083	—	74.76	.058	—	..	275	136	37	19.5	12.0	6.8	3.8	2.4	..



## STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM IN THE DIFFERENT STAGES OF THE KERR TURBINE.

STAGE 4 LOAD  $\frac{1}{4}$  BAROMETER 29.056" Hg.

PRESSURES .# GAUGE											
CALORIMETER # 1			CALORIMETER # 2			CALORIMETER # 3			STAGES		
STEAM GAUGE	WATER CONDENSED	STEAM CONDENSED	WATER DRAINED	STEAM CONDENSED	WATER DRAINED	STEAM CONDENSED	WATER DRAINED	MAIN CAL IN	IN BELOW	IN	STAGES
LB	LB	LB	LB	LB	LB	LB	LB	MAIN	MAIN	MAIN	STAGES
106.04 .021	—	73.32 .026	—	74.21 .015	—	3600 272	134	53	28.0	18.5	10.9
106.71 .023	—	73.46 .032	—	74.61 .021	—	" 274	136	52	27.3	18.1	10.5
107.34 .027	—	73.62 .040	—	75.07 .027	—	" 273	137	53	27.5	18.3	10.8
107.96 .034	—	73.72 .051	—	75.53 .037	—	" 276	132	52	27.0	18.0	10.5
108.52 .040	—	73.89 .060	—	75.95 .052	—	" 274	128	52	27.0	18.0	10.5
109.19 .049	—	74.00 .069	—	76.43 .068	—	" 271	127	52	27.4	18.2	10.8
109.85 .054	—	74.10 .082	—	76.96 .090	—	" 270	131	53	28.0	18.3	11.0

STAGE LOAD BAROMETER 29.050" HG.  
4 V<sub>2</sub>

100.67	.003	—	66.31	.040	—	65.78	.016	—	3600	273	136	73	41.5	28.0	16.5	9.0	4.7	2.0
101.40	.016	—	66.51	.057	—	66.17	.027	—	"	273	137	73	41.5	28.0	16.5	9.0	4.7	"
102.11	.028	—	66.70	.076	—	66.74	.046	—	"	279	130	74	41.0	27.5	16.0	8.9	4.6	"
102.80	.034	—	66.89	.084	—	67.25	.070	—	"	272	131	73	41.4	27.8	16.3	9.0	4.7	"
103.55	.046	—	67.06	.105	—	67.85	.095	—	"	270	138	73	41.8	28.0	16.5	9.0	4.7	"
104.19	.058	—	67.26	.115	—	68.33	.121	—	"	276	136	73	41.5	27.8	16.2	8.9	4.7	"
104.95	.070	—	67.45	.142	—	68.82	.140	—	"	274	135	73	41.5	28.0	16.2	8.9	4.7	"



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE.

STAGE 4  
LOAD  $\frac{3}{4}$   
BAROMETER 29.074 " Hg.

STAGE	LOAD	BAROMETER	29.038 " Hg.	CALORIMETER #1						CALORIMETER #2						CALORIMETER #3						PRESSURES <sup>#. GAUGE</sup>						
				STEAM CONDENSED	WATER DRAINED	R.P.M.	TEMP. IN °F	MAIN CAL	IN MAIN THROTTLE	TEMP. IN °F	MAIN CAL	IN MAIN THROTTLE	TEMP. IN °F	MAIN CAL	IN MAIN THROTTLE	TEMP. IN °F	MAIN CAL	IN MAIN THROTTLE	TEMP. IN °F	MAIN CAL								
III.68	.041	—	72.59	.034	—	72.25	.055	—	3600	273	107	98	54.0	37.5	22.0	11.5	5.8	1.4										
III.49	.050	—	72.73	.057	—	72.83	.057	—	"	272	111	96	54.5	37.0	22.0	11.7	6.0	1.4										
III.37	.069	—	73.02	.070	—	73.40	.083	—	"	270	119	95	54.0	36.3	22.0	11.6	5.8	1.3										
III.09	.093	—	73.12	.094	—	73.98	.125	—	"	272	128	94	54.0	36.0	21.5	11.5	5.5	1.3										
II.56	.116	—	73.41	.114	—	74.60	.158	—	"	274	134	95	54.5	37.0	22.0	11.7	5.6	1.3										
II.55	.129	—	73.65	.132	—	75.20	.190	—	"	278	135	94	53.5	36.0	21.3	11.4	5.5	1.3										
II.56	.149	—	73.85	.158	—	75.81	.219	—	"	279	130	93	53.0	35.5	21.0	11.4	5.4	1.3										

STAGE 4  
LOAD FULL  
BAROMETER 29.038 " Hg.

106.89	.028	—	68.94	.054	—	70.07	.043	—	3600	278	132	114	65.0	44.0	27.0	14.3	7.2	1.8										
107.89	.054	—	69.20	.098	—	70.72	.085	—	"	279	136	113	65.5	44.0	27.0	14.4	7.2	1.8										
108.72	.088	—	69.50	.144	—	71.45	.133	—	"	279	133	115	66.7	45.0	27.5	14.8	7.5	1.9										
109.62	.122	—	69.73	.180	—	72.07	.170	—	"	279	137	116	66.7	45.0	27.5	14.8	7.5	1.8										
110.46	.150	—	69.97	.217	—	72.78	.206	—	"	284	130	114	65.5	44.0	27.0	14.4	7.2	1.8										
111.62	.179	—	70.12	.25 <sup>E.T.</sup> <sub>.086</sub>	—	73.45	.258	—	"	282	126	113	66.5	45.0	27.5	14.8	7.3	1.8										
112.42	.212	—	70.40	.012	—	74.14	.072	—	"	280	122	116	67.0	45.0	28.0	15.0	8.0	2.3										

(23)



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE 5  
LOAD O  
BAROMETER 29.252" Hg.

CALORIMETER #1		STEAM		TRAP #2		CALORIMETER #3		PRESSURES		# GAUGE	
STEAM CONDENSED READING LB	WATER CONDENSED IN CONDENSER LB	TARE LB	WATER CONDENSED DRAINED LB	STEAM CONDENSED DRAINED LB	Gauge LB	WATER CONDENSED READING LB	R.P.M. MAIN	TEMP IN MAIN OF THROTTLE	IN MAIN THROTTLE	IN MAIN THROTTLE	IN MAIN THROTTLE
110.08	.178	—	523	523	—	73.40	.026	—	3600	274	137
110.51	.180	—	584	"	—	73.65	.029	—	"	271	126
111.00	.182	—	649	"	—	73.90	.031	—	"	264	120
111.46	.183	—	704	"	—	74.22	.037	—	"	260	116
111.97	.186	—	764	"	—	74.45	.040	—	"	254	112
112.44	.187	—	825	"	—	74.78	.045	—	"	251	117
112.85	.188	—	885	"	.25	75.07	.050	—	"	255	118

STAGE 5  
LOAD  $\frac{1}{4}$   
BAROMETER 29.252" Hg.

110.45	.143	—	540	540	—	69.67	.037	—	3600	265	121	52	27.5	18.0	10.6	6.2	3.7	2.1
110.97	.145	—	611	"	—	70.02	.039	—	"	262	121	53	28.0	"	11.0	6.4	"	2.1
111.51	.155	—	699	"	—	70.35	.045	—	"	263	123	53	28.0	"	10.9	6.4	"	2.2
112.04	.160	—	776	"	—	70.70	.050	—	"	264	123	53	28.0	"	10.9	6.4	"	2.2
112.70	.161	—	875	"	—	71.10	.054	—	"	262	127	53	28.0	"	11.0	6.4	"	2.2
113.08	.164	—	942	"	—	71.40	.057	—	"	262	131	53	28.0	"	11.0	6.4	"	2.2
113.63	.167	—	1019	"	.31	71.72	.060	—	"	262	140	54	28.0	"	11.0	6.5	"	2.3



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE 5  
LOAD  $\frac{1}{2}$   
BAROMETER 29.232 " Hg.

CALORIMETER #1	STEAM.			TRAP #2			CALORIMETER #3			PRESSURES						# CHANGES
	STEAM GAUGE	WATER CONDENSER DRAINED	TARE LB	WATER CONDENSER IN CONDENSER LB	STEAM DRAINED	CONDENSED READING LB	WATER GAUGE	WATER DRAINED	CONDENSED READING LB	R.P.M.	IN MAIN CAL	IN MAIN	IN MAIN THROTTLE	IN MAIN	IN MAIN	
108.88	.092	—	582	582	—	73.61	.025	—	3600	261	117	74	42.0	27.9	16.5	9.2 4.7 2.1
109.48	.104	—	693	"	—	74.00	.029	—	"	258	127	75	42.0	28.0	16.8	9.2 "
110.03	.107	—	794	"	—	74.44	.040	—	"	257	140	75	42.5	28.0	16.8	9.2 "
110.65	.119	—	909	"	—	74.88	.058	—	"	266	133	75	42.0	27.7	16.5	9.2 "
111.26	.121	—	1016	"	—	75.31	.070	—	"	264	135	75	42.0	27.5	16.2	9.1 "
112.00	.123	—	1127	"	—	75.71	.088	—	"	266	133	75	42.0	28.0	16.3	9.1 "
112.47	.126	—	1252	"	.52	76.14	.109	—	"	269	131	74	42.0	28.0	16.1	9.1 "

STAGE 5  
LOAD  $\frac{3}{4}$   
BAROMETER 29.204 " Hg.

104.64	.072	—	492	492	—	70.63	.025	—	3600	270	133	96	55.0	37.0	22.0	12.0	6.0	2.0
105.24	.080	—	635	"	—	71.03	.030	—	3580	271	136	97	55.0	37.0	22.0	"	"	"
105.87	.090	—	768	"	—	71.56	.038	—	3600	270	140	96	54.5	36.0	22.0	"	"	"
106.58	.095	—	904	"	—	72.00	.040	—	3600	274	137	96	54.5	36.0	22.0	"	"	"
107.23	.102	—	1055	"	—	7245	.049	—	3600	275	135	94	54.5	36.0	22.0	"	"	"
107.88	.104	—	1194	"	—	72.83	.060	—	3600	277	128	95	54.5	36.0	22.0	"	"	"
108.51	.110	—	1346	"	.39	73.37	.072	—	3600	275	124	96	54.0	36.2	22.1	"	"	"



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

5  
FULL  
LOAD  
BAROMETER 29.278" Hg.

CALORIMETER #1	STEAM			TRAP #2			CALORIMETER #3			PRESSURES										
	STEAM GAUGE	WATER CONDENSED	TARE	WATER DRAINED	STEAM CONDENSED	GAUGE	WATER DRAINED	CONDENSED	READING	WATER DRAINED	MAIN CAL OF	IN MAIN	IN BELOW THROTTLE	IN STAGES	# GAUGE					
	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	OF	MAIN	MAIN	THROTTLE	1	2	3	4	5	6
110.85	.040	—	650	650	—	74.89	.046	—	3600	279	132	118	67.5	45.0	28.0	15.0	8.0	2.1		
111.53	.046	—	812	"	—	75.39	.050	—	3600	278	127	117	67.5	46.0	"	15.2	"	2.1		
112.26	.052	—	977	"	—	75.95	.057	—	3600	278	122	115	67.2	46.0	"	15.2	"	2.2		
113.04	.058	—	1148	"	—	76.50	.069	—	3600	276	124	120	68.0	46.0	"	15.2	"	2.3		
113.75	.061	—	1317	"	—	77.02	.080	—	3570	277	123	116	67.8	46.0	"	15.1	"	2.2		
114.46	.064	—	1474	"	—	77.51	.091	—	3600	276	123	118	68.0	46.0	"	15.2	"	2.2		
114.18	.066	—	1627	"	43	78.12	.118	—	3600	276	127	117	67.5	45.0	"	15.0	"	2.2		

6  
O  
LOAD  
BAROMETER 29.142" Hg.

CALORIMETER #1	STEAM			TRAP #2			CALORIMETER #3			PRESSURES										
	STEAM GAUGE	WATER CONDENSED	TARE	WATER DRAINED	STEAM CONDENSED	GAUGE	WATER DRAINED	CONDENSED	READING	WATER DRAINED	MAIN CAL OF	IN MAIN	IN BELOW THROTTLE	IN STAGES	# GAUGE					
	LB	LB	LB	LB	LB	LB	LB	LB	LB	LB	OF	MAIN	MAIN	THROTTLE	1	2	3	4	5	6
102.61	.140	—	548	548	—	78.55	.050	—	3620	251	120	40	20.0	13.0	8.2	4.7	3.4	2.1		
103.12	.141	—	607	"	—	78.84	.052	—	3630	257	122	"	20.0	13.0	8.0	4.7	3.4	2.1		
103.56	.145	—	674	"	—	79.10	.056	—	3618	254	119	"	20.0	13.7	8.0	4.5	3.2	2.0		
104.00	.148	—	734	"	—	79.38	.060	—	3600	248	120	"	20.0	13.0	8.0	4.5	3.3	2.0		
104.47	.150	—	797	"	—	79.68	.068	—	3600	248	120	"	20.0	13.0	8.0	4.5	3.2	2.0		
104.94	.154	—	863	"	—	79.91	.070	—	3600	251	122	"	20.5	13.0	8.2	4.6	3.2	2.1		
105.37	.155	—	925	"	.11	80.20	.077	—	3620	254	120	"	20.0	13.8	8.0	4.5	3.2	2.1		



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE

LOAD  
BAROMETER  $\frac{1}{4}$

6  
BAROMETER 29.136" Hg.

CALORIMETER #1	STEAM			TRAP #2		CALORIMETER #3		TEMP IN MAIN WATER CIRCUIT OF R.P.M	PRESSURES # GAUGE IN STAGES
	STEAM CONDENSED WATER DRAINED LB	WATER CONDENSED IN CONDENSER LB	TARE LB	WATER DRAINED LB	STEAM CONDENSED LB	WATER DRAINED LB	IN MAIN THROTTLE		
103.58 .052	—	560	560	—	76.40	.033	—	3600	252
104.00 .057	—	648	"	—	76.72	.039	—	3600	253
104.46 .062	—	720	"	—	76.94	.040	—	3625	256
104.90 .077	—	810	"	—	77.22	.047	—	3620	257
105.41 .081	—	890	"	—	77.50	.052	—	3635	258
105.82 .090	—	972	"	—	77.77	.056	—	3600	261
106.27 1.04	—	1048	"	.14	78.01	.060	—	3600	259

STAGE  
LOAD  
BAROMETER

6  
 $\frac{1}{2}$   
BAROMETER 29.090" Hg.

105.05 .052	—	1020	1020	—	74.34	.051	—	3600	252
105.56 .060	—	1138	"	—	74.65	.060	—	3620	251
106.00 .068	—	1253	"	—	74.88	.070	—	3600	249
106.47 .074	—	1370	"	—	75.18	.077	—	3600	252
106.95 .076	—	1484	"	—	75.48	.070	—	3600	257
107.42 .085	—	1606	"	—	75.81	.084	—	3625	260
107.87 .080	—	1715	"	.23	76.15	.100	—	3600	260



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

STAGE 6  
LOAD  $\frac{3}{4}$   
BAROMETER 29.078" Hg.

CALORIMETER #1		STEAM		TRAP #3		CALORIMETER #3		TEMP IN MAIN CH.		PRESSURES IN STAGES					
STEAM GAUGE	WATER CONDENSED	WATER DRAINED	CONDENSER TARE	STEAM GAUGE	CONDENSED	WATER DRAINED	R.P.M.	IN MAIN CH. °F	IN MAIN THROTTLE	1	2	3	4	5	6
LB	LB	LB	LB	LB	LB	LB									
107.36	.025	—	507	507	—	75.69	.021	—	3575	267	125	95	53.5	35.0	21.6
107.85	.029	—	655	..	—	75.95	.026	—	3600	268	129	94	54.0	35.0	21.5
108.26	.034	—	789	..	—	76.23	.028	—	3600	267	130	93	54.0	35.0	21.8
108.70	.038	—	945	..	—	76.50	.033	—	3600	269	130	92	53.5	35.0	21.0
109.13	.045	—	1060	..	—	76.73	.046	—	3600	272	122	93	53.5	35.2	21.6
109.59	.067	—	1205	..	—	77.00	.057	—	3600	270	117	93	53.8	35.5	21.6
110.03	.073	—	1345	..	.20	77.26	.076	—	3600	268	118	94	54.0	35.8	21.9

STAGE 6  
LOAD FULL  
BAROMETER 29.070" Hg.

100.71	.025	—	597	597	—	75.16	.023	—	3600	275	134	114	66.0	44.5	27.3	14.8	7.9	2.1
101.14	.029	—	758	..	—	75.30	.029	—	"	274	138	113	66.0	44.0	27.0	14.8	8.0	2.1
101.68	.034	—	943	..	—	75.60	.035	—	"	274	138	113	67.0	45.0	28.0	15.0	8.0	2.1
102.16	.048	—	1093	..	—	75.87	.039	—	"	280	128	114	65.0	43.5	27.0	14.5	7.6	2.0
102.62	.050	—	1259	..	—	76.12	.049	—	"	277	127	113	66.0	44.0	27.0	14.8	7.7	2.0
103.13	.058	—	1427	..	—	76.42	.062	—	"	272	136	114	66.0	44.4	27.5	14.9	7.8	2.0
103.61	.062	—	1589	..	.18	76.67	.071	—	"	279	134	113	66.0	44.2	27.5	14.8	7.7	2.0



STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE

RESULT SHEET # 1

No	NOTATION	PRELIMINARY TESTS						STAGE #1			STAGE #2			STAGE #3		
		0	1/4	1/2	3/4	FULL	3	1/4	1/2	3/4	FULL	0	1/4	1/2	3/4	FULL
1	LOAD	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
2	LOAD IN B.H.P.	0.0	9.6	19.27	28.9	38.6	0.0	9.56	19.27	28.9	—	0.0	9.6	19.27	28.9	38.6
3	CAL#1. WEIGHT OF CONDENSED STEAM LB	—	—	—	—	—	5.31	9.30	4.28	11.82	—	0.0	9.6	19.27	28.9	—
4	" WEIGHT OF SEPARATED WATER LB	—	—	—	—	—	.028	.123	.101	.196	—	.422	5.04	7.34	8.66	—
5	" WEIGHT OF SEPARATED WATER LB BY WEIGHING.	—	—	—	—	—	—	—	—	—	—	.084	.302	.568	.888	—
6	CAL#2. WEIGHT OF CONDENSED STEAM LB	—	—	—	—	—	2.38	3.44	9.11	5.63	—	—	3.37	.578	.945	—
7	" WEIGHT OF SEPARATED WATER LB	—	—	—	—	—	.016	.062	.191	.114	—	.221	.495	.979	1.432	—
8	" WEIGHT OF SEPARATED WATER LB BY WEIGHING.	—	—	—	—	—	—	—	—	—	—	.225	.519	1.097	.1632	—
9	CAL#3. WEIGHT OF CONDENSED STEAM LB	—	—	—	—	—	3.81	5.55	7.11	8.67	—	3.15	4.10	.542	.63	—
10	" WEIGHT OF SEPARATED WATER LB	—	—	—	—	—	.016	.096	.211	.249	—	.111	.241	.30	.368	—
11	" WEIGHT OF SEPARATED WATER LB BY WEIGHING	—	—	—	—	—	—	—	—	—	—	.23	.31	.433	—	—
12	WEIGHT OF EXHAUST STEAM. LB.	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
13	WEIGHT OF WATER TO TRAP, LB.	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
14	PRESSURE IN MAIN. # GAUGE.	—	—	—	—	—	134.6	121.4	128.4	126.3	—	133.4	126.8	131.3	124	—
15	" BELOW THROTTLE "	30.943	52.3	70	93.4	114.3	34.86	54.0	77.0	96.7	—	35.43	52.0	73.0	95.6	—
16	IN FIRST STAGE	16.686	27.26	40.93	54.07	67.0	16.7	27.3	41.43	54	—	17.0	26.97	40.5	54.26	—
17	" SECOND "	10	17.64	26.886	35.37	45.2	9.93	18.57	27.71	36.2	—	10.0	17.5	26.6	35.4	—
18	" THIRD "	6.14	10.7	16.0	21.986	28	5.21	10.50	16.06	22.03	—	5.1	10.34	15.43	21.24	—
19	" FOURTH "	3.83	6.086	8.93	11.814	15	2.8	5.64	8.76	11.93	—	2.87	6.0	3.71	11.76	—
20	" FIFTH "	2.89	3.686	4.73	6.0	8.0	1.28	3.54	4.7	6.63	—	1.13	3.6	3.73	6.04	—
21	" SIXTH "	2.04	2.0	1.9	2.0	0.0	1.5	1.9	2.41	—	0.0	1.914	1.986	1.96	—	.73
22	BAROMETER READING : INCHES HG	—	—	—	—	—	28.791	29.469	29.471	28.790	—	28.873	28.864	28.860	—	29.196
23	TEMPERATURE IN MAIN CALORIFIER °F	—	—	—	—	—	280.1	271.3	274.1	279.86	—	278.0	273.4	274.6	279	—
24	REV. PER. MIN.	3600	3600	3600	3600	3600	3592	3600	3600	3600	—	3600	3600	3600	3600	3600
25	LENGTH OF BRAKE ARM IN FT.	2.5	2.5	2.5	2.5	2.5	—	—	—	—	—	2.5	2.5	2.5	2.5	2.5
26	WEIGHT ON BRAKE SCALE. LB.	0.0	5.6	11.25	16.87	22.5	0.0	5.6	11.25	16.87	—	0.0	5.6	11.25	16.87	22.5
27	TARE WEIGHT OF BRAKE ON SCALE. LB	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	—	34.4	34.4	34.4	34.4	34.4
28	QUALITY OF STEAM IN CAL#1 = X <sub>1</sub>	—	—	—	—	—	.996	.986	.982	.985	—	.981	.937	.9275	.901	—
29	" " " "#2 = X <sub>2</sub>	—	—	—	—	—	.995	.955	.827	.98	—	.892	.825	.794	.961	—
30	" " " "#3 = X <sub>3</sub>	—	—	—	—	—	.996	.956	.910	.972	—	.965	.947	.936	.995	.975
31	MEAN QUALITY IN STAGE.	—	—	—	—	—	.996	.966	.906	.979	—	.946	.963	.889	.933	.967
32	QUALITY IN MAIN.	—	—	—	—	—	.987	.985	.984	.988	—	.985	.983	.988	.981	.986

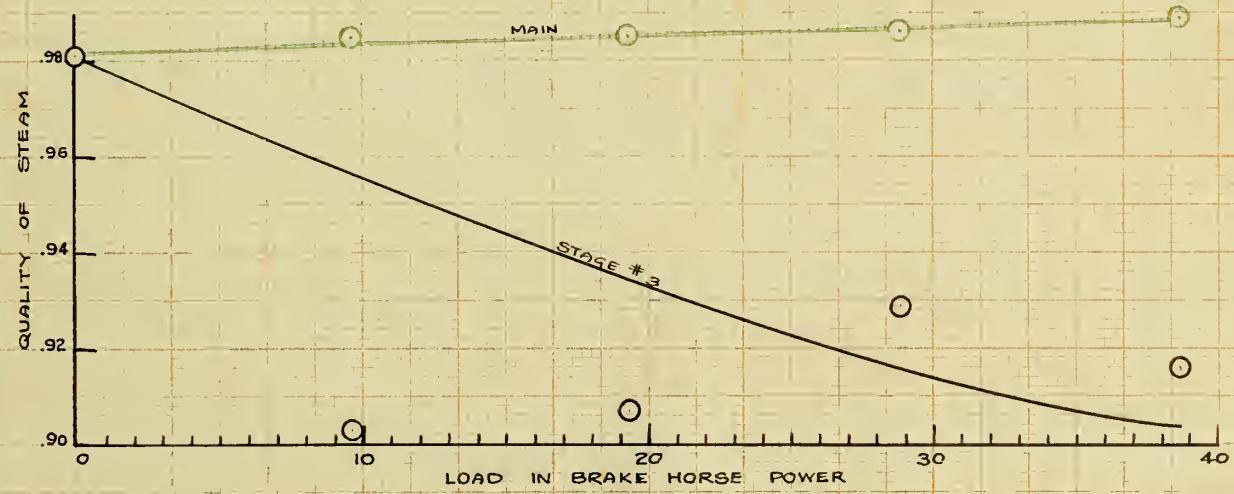
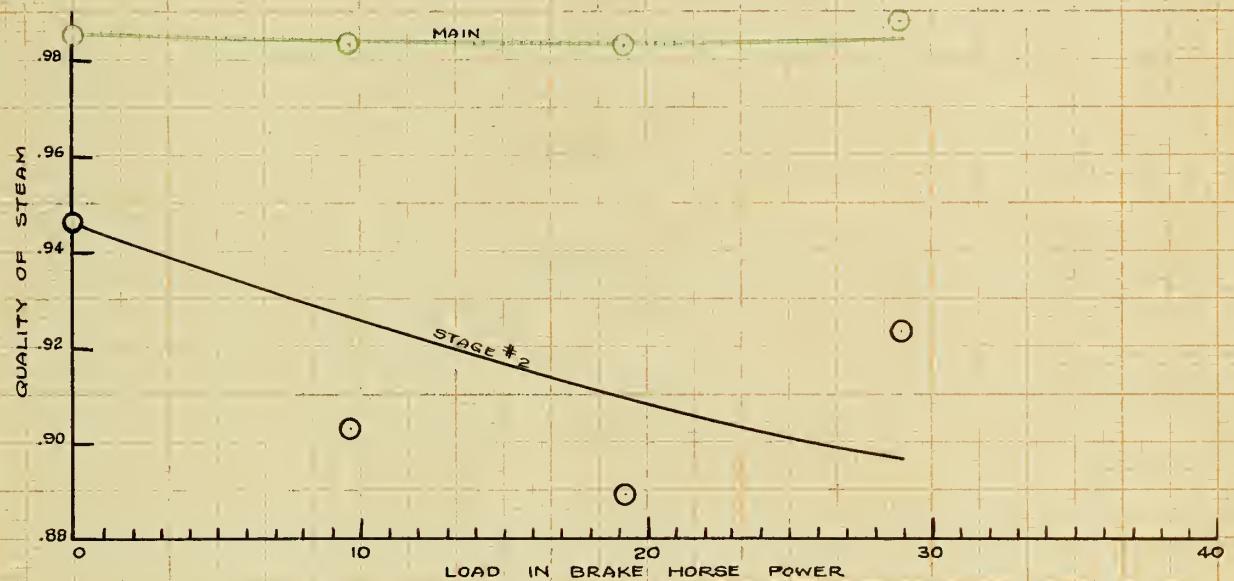
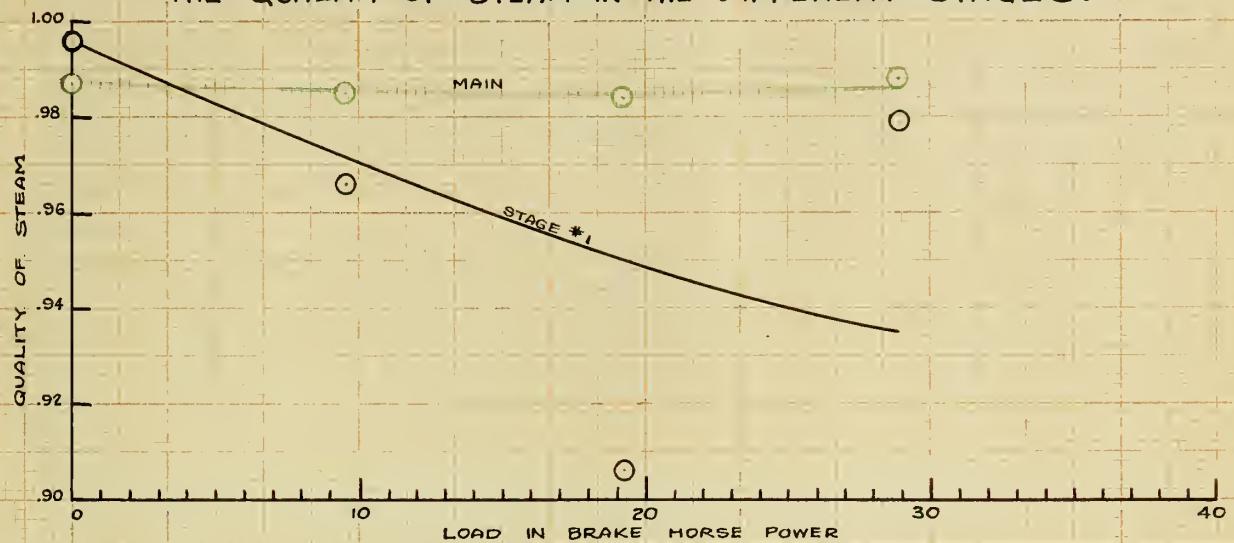


STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
IN THE DIFFERENT STAGES OF THE KERR TURBINE.  
RESULT SHEET #2.

No	NOTATION	PRELIMINARY TESTS				STAGE #4				STAGE #5				STAGE #6							
1	LOAD	0	1/4	1/2	3/4	FULL	0	1/4	1/2	3/4	FULL	0	1/4	1/2	3/4	FULL					
2	LOAD IN B.H.P.	0.0	9.6	19.27	28.9	38.6	0.0	9.6	19.27	28.9	38.6	0.0	9.62	19.29	28.87	38.6					
3	CAL#1. WEIGHT OF CONDENSED STEAM LB	—	—	—	—	—	3.30	3.81	3.52	4.88	5.53	2.77	3.18	3.59	3.86	3.33	2.76	2.69	2.82	2.67	2.90
4	" WEIGHT OF SEPARATED WATER LB	—	—	—	—	—	0.22	0.33	0.55	1.08	1.84	.01	.024	.034	.038	.026	.015	.052	.028	.048	.037
5	" WEIGHT OF SEPARATED WATER LB BY WEIGHING	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
6	CAL#2. WEIGHT OF CONDENSED STEAM LB	—	—	—	—	—	.61	.78	.95	1.26	1.46	—	—	—	—	—	—	—	—	—	—
7	" WEIGHT OF SEPARATED WATER LB	—	—	—	—	—	.05	.056	.075	.124	.23	—	—	—	—	—	—	—	—	—	—
8	" WEIGHT OF SEPARATED WATER LB BY WEIGHING	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
9	CAL#3. WEIGHT OF CONDENSED STEAM LB	—	—	—	—	—	2.33	2.75	3.04	3.56	4.07	1.67	2.05	2.53	2.74	3.23	1.65	1.61	1.81	1.57	1.51
10	" WEIGHT OF SEPARATED WATER LB	—	—	—	—	—	.041	.075	.124	.164	.241	.024	.023	.084	.047	.072	.027	.049	.055	.048	—
11	" WEIGHT OF SEPARATED WATER LB BY WEIGHING	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
12	WEIGHT OF EXHAUST STEAM LB	—	—	—	—	—	—	—	—	—	—	36.2	47.9	67.0	854	977	377	488	695	838	992
13	WEIGHT OF WATER TO TRAP LB	—	—	—	—	—	—	—	—	—	—	.22	.27	.45	.34	.37	.096	.122	.262	.17	.157
14	PRESSURE IN MAIN - # GAUGE.	—	—	—	—	—	137.5	132.1	134.8	123.4	130.86	120.86	126.5	130.85	133.3	125.43	120.5	125.43	121.4	124.4	133.6
15	" BELOW THROTTLE "	30.943	52.3	70	93.4	114.3	36.6	52.4	73.14	95.0	114.4	37.3	53.0	74.7	95.6	117.3	40.0	52.0	74.85	93.4	113.43
16	" IN FIRST STAGE	16.486	27.26	40.93	54.07	67.0	8.87	27.46	41.46	53.93	66.13	19.3	27.93	42.07	54.7	67.64	20.07	27.0	42.2	53.75	66.0
17	" " SECOND "	10.0	17.64	26.886	35.37	45.2	12.14	18.2	27.88	36.47	44.6	12.13	18.0	27.87	36.3	45.7	12.92	17.34	27.8	35.7	44.23
18	" " THIRD "	6.14	10.7	16.0	21.986	28.0	6.86	10.71	16.31	21.7	27.36	7.3	10.91	16.45	22.01	28.0	8.06	10.41	16.5	21.6	27.33
19	" " FOURTH "	3.83	6.086	8.93	11.814	15.0	3.79	5.98	8.96	11.55	14.64	4.43	6.4	9.16	12.0	15.13	4.57	5.97	9.17	11.63	14.8
20	" " FIFTH "	2.9	3.686	4.73	6.0	8.0	2.44	3.57	4.69	5.66	7.41	3.0	3.7	4.7	6.0	8.0	3.27	3.6	4.91	6.0	7.81
21	" " SIXTH "	2.04	2.0	1.9	2.0	.9	1.86	2.0	1.33	1.88	1.8	2.18	2.1	2.0	2.18	2.06	2.0	2.0	1.98	2.04	
22	BAROMETER READING. INCHES HG.	—	—	—	—	—	79.154	79.056	79.05	79.074	79.038	29.252	29.232	29.204	29.278	29.142	29.136	29.09	29.078	29.070	
23	TEMPERATURE IN MAIN CALORIMETER °F	—	—	—	—	—	277.8	272.88	273.96	274	280.1	261.3	263.0	273.1	277.1	252	256.6	254.4	268.7	276	—
24	REV. PER. MIN.	3600	3600	3600	3600	3600	3600	3600	3600	3600	3600	3600	3600	3600	3600	3600	3606	3606	3597	3600	
25	LENGTH OF BRAKE ARM IN FEET	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	2.5	
26	WEIGHT ON BRAKE SCALE - TARE LB	0.0	5.6	11.25	16.87	22.5	0.0	5.6	11.25	16.87	22.5	0.0	5.6	11.25	16.87	22.5	0.0	5.6	11.25	16.87	22.5
27	TARE WEIGHT ON BRAKE SCALES LB	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	34.4	
28	QUALITY OF STEAM IN CAL#1 X1	—	—	—	—	—	.994	.992	.985	.980	.968	.997	.992	.998	.995	.992	.995	.9935	.990	.978	.989
29	" " " #2 = X2	—	—	—	—	—	.925	.934	.927	.911	.865	—	—	—	—	—	—	—	—	—	—
30	" " " #3 = X3	—	—	—	—	—	.983	.974	.960	.955	.945	.987	.990	.984	.980	.985	.975	.967	.971	—	—
31	MEAN QUALITY IN STAGE	—	—	—	—	—	.967	.966	.957	.949	.926	.992	.990	.979	.988	.980	.990	.965	.982	.973	.980
32	QUALITY IN MAIN.	—	—	—	—	—	.985	.984	.983	.985	.986	.980	.979	.978	.984	.973	.976	.974	.982	.984	(30)

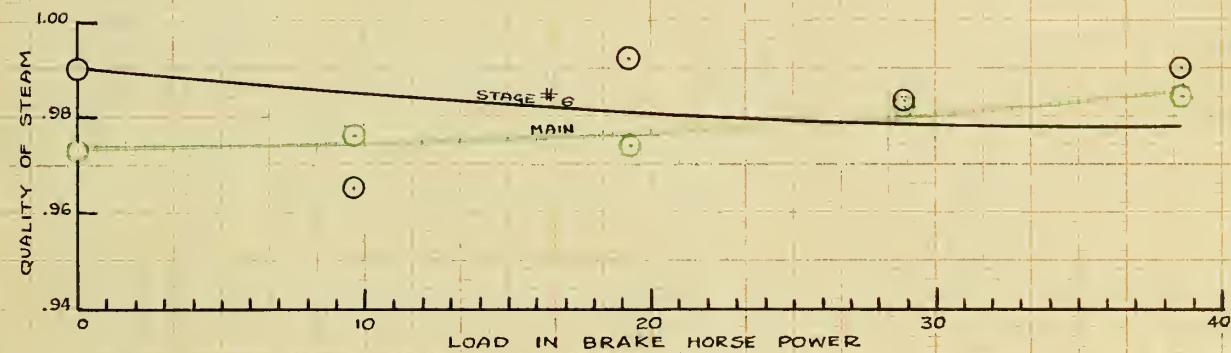
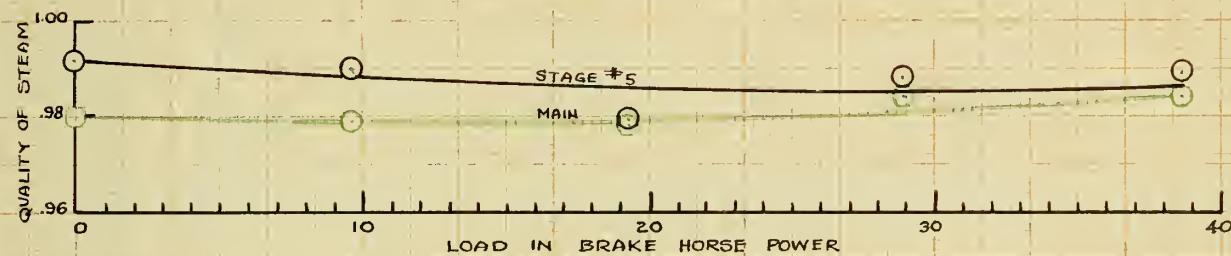
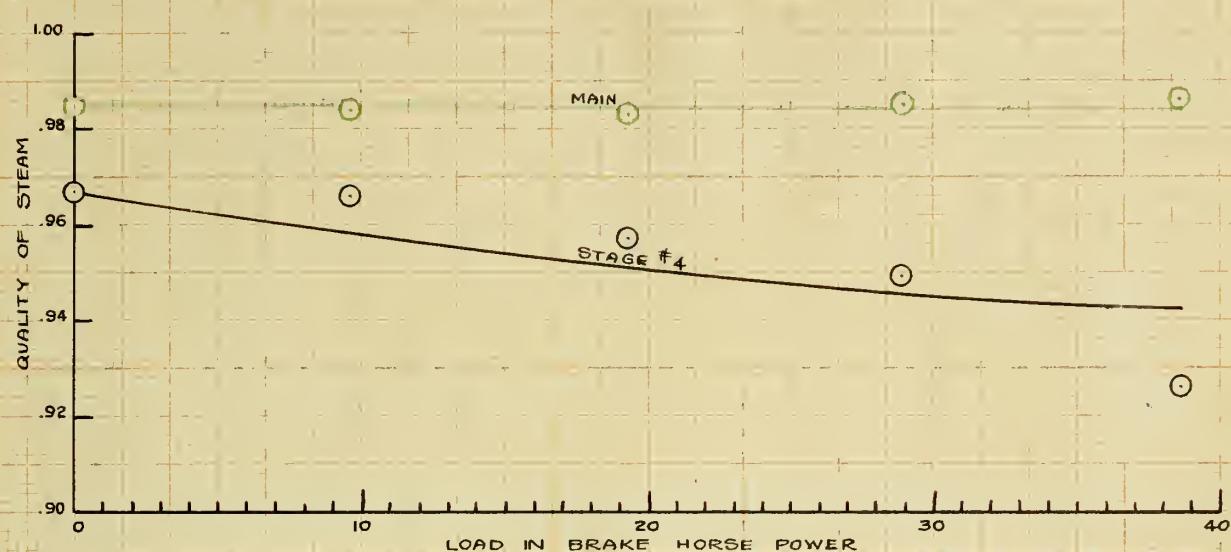


STUDY IN THE VARIATION IN THE QUALITY OF THE STEAM  
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CURVES SHOWING RELATION BETWEEN LOAD IN B.H.P. AND  
THE QUALITY OF STEAM IN THE DIFFERENT STAGES.



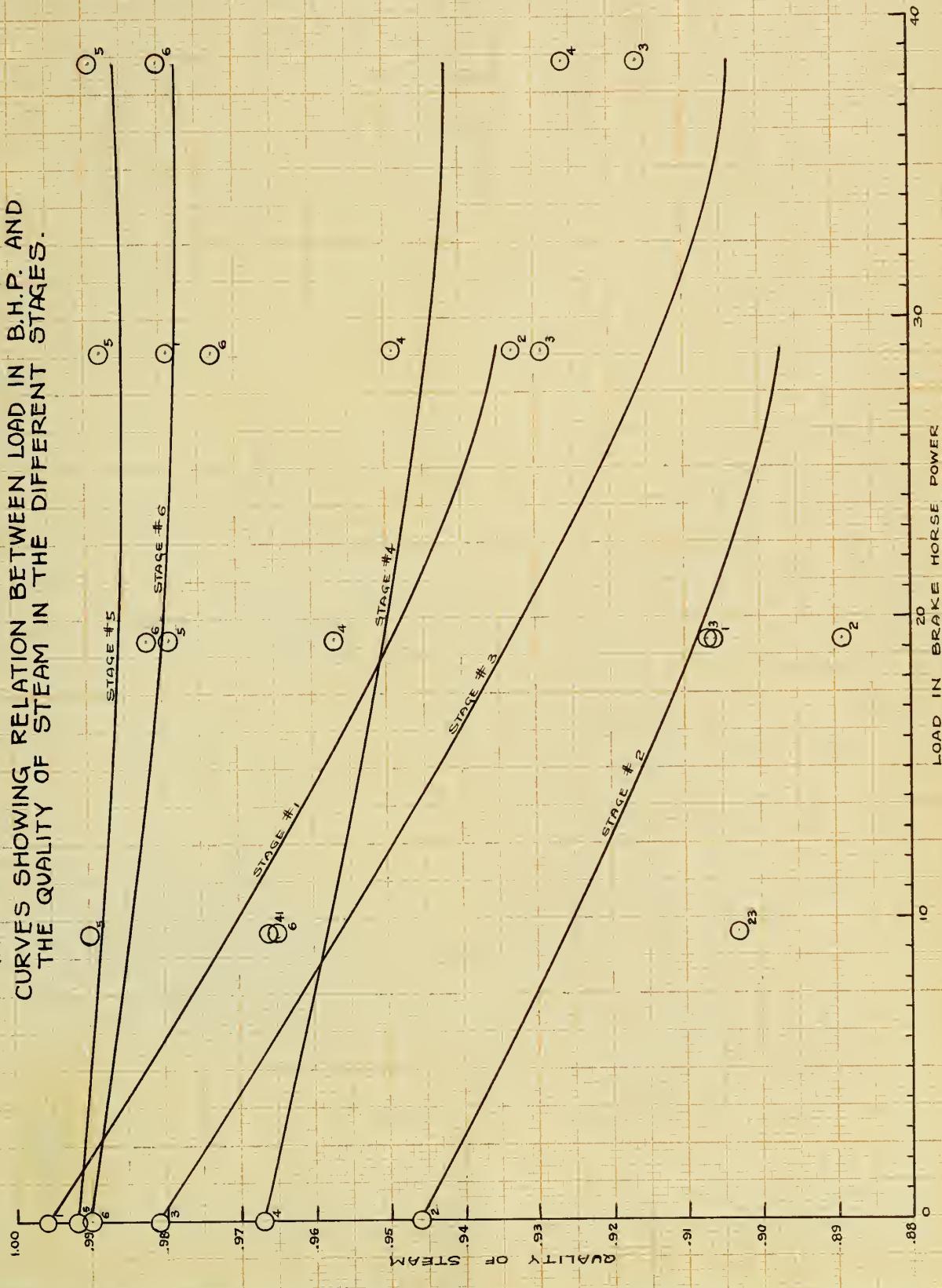


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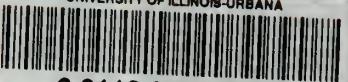
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